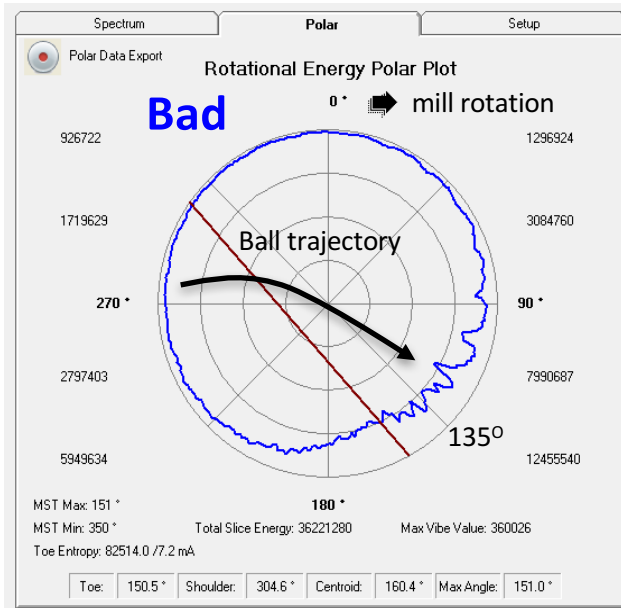
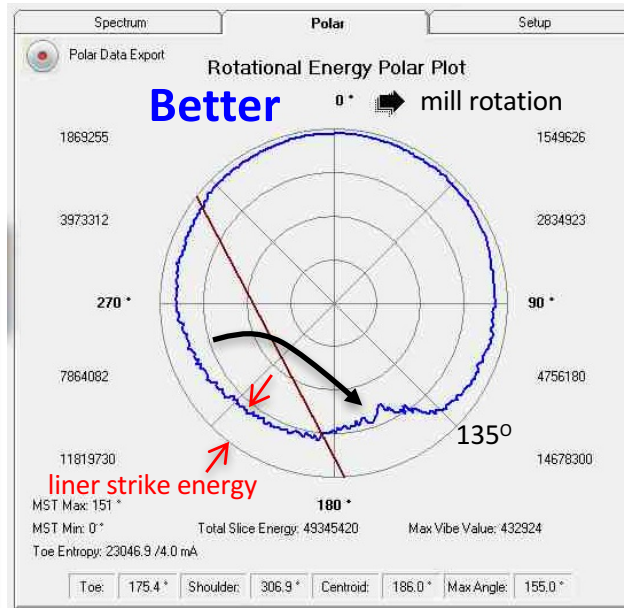


# Barrick GoldStrike Operator's Guide - MillSlicer Polar Plot Analysis



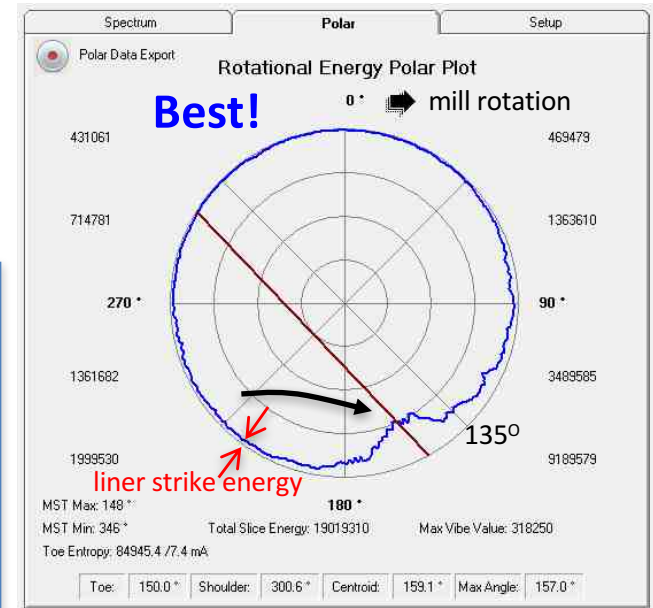
Case 1. **Empty Mill w/Excessive RPMs**

- Mill is rotating in a clockwise direction
- Sensor on shell measures vibration energy in the full rotation and energy is plotted increasing toward the center of the plot
- **RPMs are too high** so balls **strike high** on the opposite side of the liner causing sharp energy peaks from 90 – 135 degrees.
- **Extreme excessive wear/damage to the liners**



Case 2. **Empty Mill w/Good RPMs**

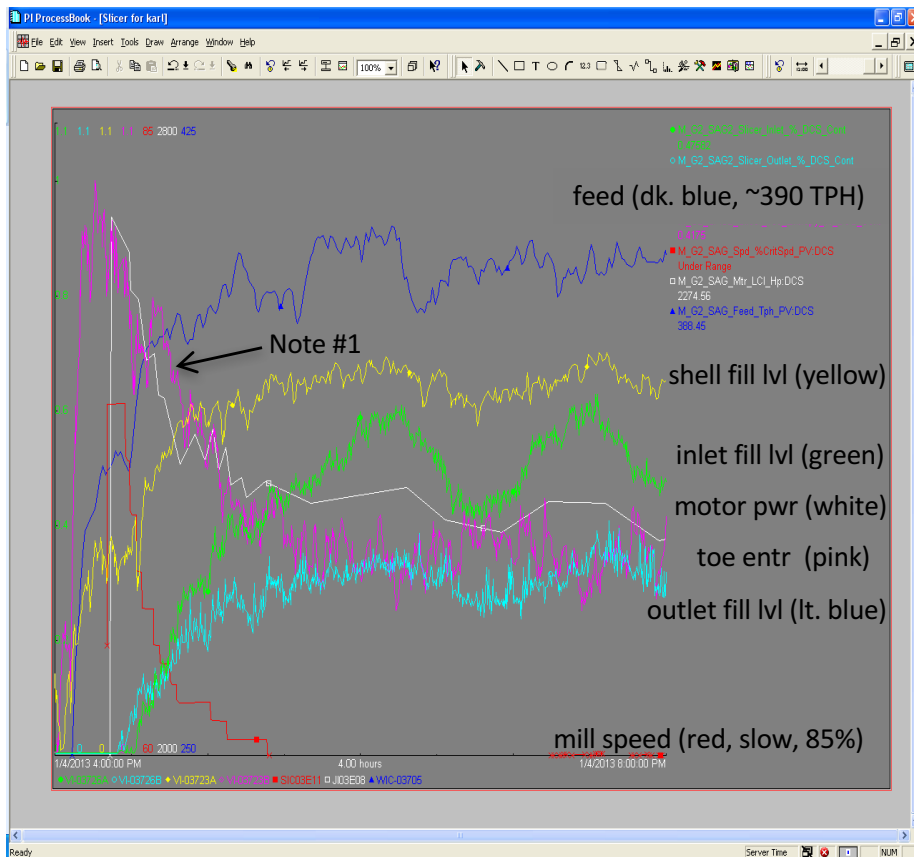
- Snap shot taken on a mill being ground out at low speed (85% speed)
- No sharp peaks from 90 – 135 degrees which is good
- Liner strike energy from 135 – 270 degrees is high but there is nothing we can do about this, it is a result of the mill being empty
- **Grind-outs should be always done at low speeds (80-85%) by cutting the feed**



Case 3. **Full Mill & Cascade Grinding**

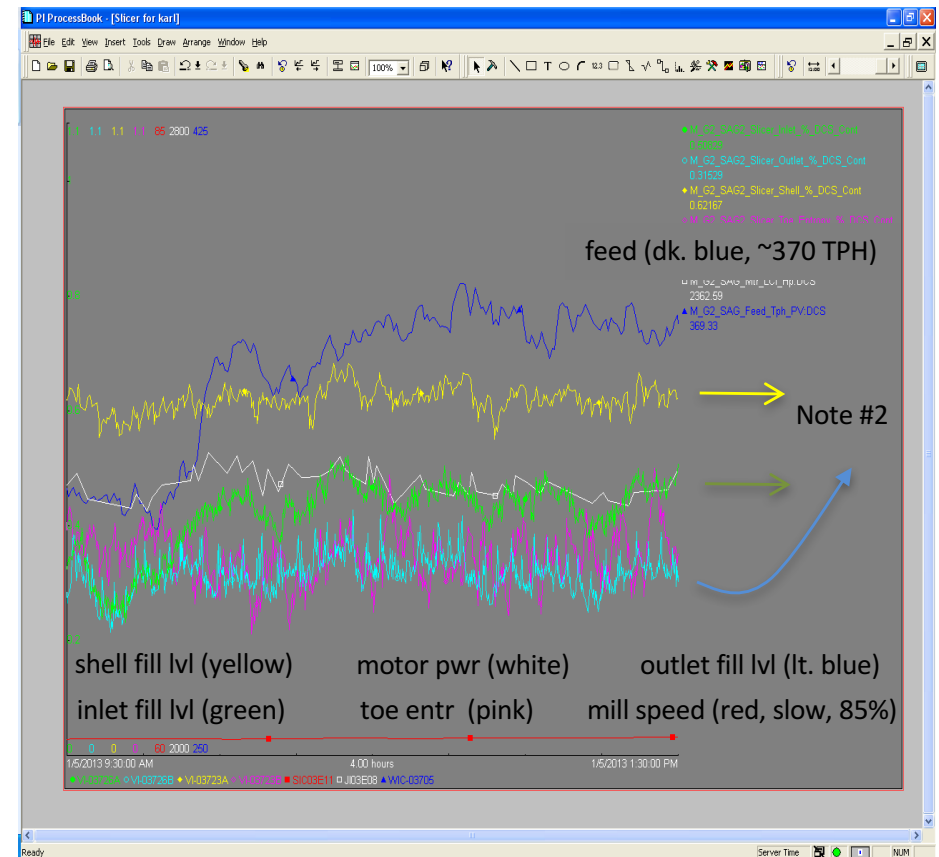
- When the mill begins to fill to levels above 50% on the shell sensor fill level trend, we see a **focusing of the grinding energy** in the region from 135 – 180 degrees
- Optimal cascade grinding is occurring and we are operating the SAG mill per it's intended design
- Ball to liner strike energy significantly reduces to very low levels. i.e. compare the liner strike energy between Cases 2 and 3 from 180 – 270 degrees
- **Optimal grinding & minimal liner damage!**

# MineralScan MillSlicer Trend Summary – Inlet, Outlet, Shell Vibration Sensors



## Case 1. Mill Start-up from Grind-out w/Reduced Speed

- This trend was taken from the SAG upon start up where the feed was brought up first and then the speed was decreased to retain material.
- When all three fill level signals track one another, the material entering the mill = the material leaving the mill. **This is good stable operation!**
- Note #1: Toe Entropy (pink) is a measure of how hard the balls are striking the mill shell. 100% = Very bad liner damage, 0% = minimal liner damage. **This signal should be kept under 50% if possible.**



## Case 2. Stable Operation w/Reduced Speed

- Like the trend on the left, **the goal is to flatten all three fill level signals** (inlet, shell, outlet). When all three sensor signals are flat, we can begin to further fill the mill by either increasing feed or reducing mill speed. This should then result in **all three signals stepping up together in a uniform manner which is the desired method to slowly step fill the mill. The shell sensor polar plot should also be used to indicate a full mill.**
- Note #2: Due to temperature limitations, the SAG mill could not be run at its maximum intended feed rate (590+ TPH) and filled to high fill levels. However if there were no limitations and the mill were to overflow, we can immediately detect this **by observing that the outlet signal (lt. blue) takes off upward in comparison to the other fill levels. The output signal should therefore be used to detect blockages.**



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